

# Modelling optimal ligninolytic activity during plant litter decomposition

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## Summary

- A large fraction of plant litter comprises recalcitrant aromatic compounds (lignin and other phenolics). Quantifying the fate of aromatic compounds is difficult, because oxidative degradation of aromatic carbon (C) is a costly but necessary endeavor for microorganisms, and we do not know when gains from the decomposition of aromatic C outweigh energetic costs.
- To evaluate these tradeoffs, we developed a litter decomposition model in which the aromatic C decomposition rate is optimized dynamically to maximize microbial growth for the given costs of maintaining ligninolytic activity. We tested model performance against > 200 litter decomposition datasets collected from published literature and assessed the effects of climate and litter chemistry on litter decomposition.
- The model predicted a time-varying ligninolytic oxidation rate, which was used to calculate the lag time before the decomposition of aromatic C is initiated. Warmer conditions increased decomposition rates, shortened the lag time of aromatic C oxidation, and improved microbial C-use efficiency by decreasing the costs of oxidation. Moreover, a higher initial content of aromatic C promoted an earlier start of aromatic C decomposition under any climate.
- With this contribution, we highlight the application of eco-evolutionary approaches based on optimized microbial life strategies as an alternative parametrization scheme for litter decomposition models.

## Introduction

The question of whether the decomposition of complex polymers, such as lignin and similar compounds, represents a significant rate-limiting step to terrestrial carbon (C) cycling has been a subject of extensive research. However, a gap in understanding of the mechanistic controls on the decomposition of these recalcitrant compounds remains (Thevenot *et al.*, 2010; Hall *et al.*, 2020). Plant detritus, exudates, and their derived compounds are building blocks of particulate and mineral-associated organic matter (Huang *et al.*, 2019; Cotrufo & Lavelle, 2022). Therefore, accurate predictions of decomposition rates of these litter components are crucial for better understanding the fate of C in soils (Moorhead & Sinsabaugh, 2006). Moreover, litter decomposition releases essential plant nutrients, and in some ecosystems, low decomposition rates contribute to retention of nutrients in recalcitrant pools. However, the timing of lignin decomposition, the associated release of lignin-protected compounds, and the tradeoffs with other microbial functions are not well understood, leaving uncertainties regarding incorporation of litter-derived organic matter into the soil and nutrient release during decomposition. Much of the lignin is released as CO<sub>2</sub> during decomposition as mainly basidiomycete fungi degrade it to get access to energy and nutrient-rich compounds, and part of

it may also be used to fuel fungal growth (Berg & McClaugherty, 1987; Kirk & Farrell, 1987; del Cerro *et al.*, 2021). In particular, uncertainty surrounding the temperature sensitivity of decomposition rates of lignin-like compounds in aboveground litter, topsoil, and subsoil hinders our capacity to quantify the persistence of soil organic C in future warming scenarios (Allison *et al.*, 2018; Chen *et al.*, 2020; Tan *et al.*, 2020; Dao *et al.*, 2022; Zosso *et al.*, 2023).

Much of the uncertainties in assessing the dynamics of lignin decomposition are associated with unknown constraints on fungal communities with ligninolytic capacities. Vivello & Bhatnagar (2019) suggested that ‘decomposer fungal succession is partially rooted in fungal decomposers’ deep evolutionary history’, implying that microbial activity might be regulated according to evolutionary pressures toward improved fitness. Indeed, the succession of different microbial groups linked to different extracellular enzyme activities is correlated with mass loss of different litter fractions, suggesting that different microbial guilds contribute to the degradation of complex compounds (Šnajdr *et al.*, 2011; Bhatnagar *et al.*, 2018). These community composition dynamics are shaped by microbial succession linked to litter chemical traits (specifically nutrient content and the abundance of recalcitrant compounds) and their interaction with local soil conditions. Together, litter quality and soil properties modulate the activities

of community members in controlling litter decomposition (Buresova *et al.*, 2019; Herzog *et al.*, 2019). Additionally, extracellular enzyme activities change during litter decomposition, even when litter is colonized by a single fungus (Barbi *et al.*, 2020). Thus, decomposition is regulated by both community-level changes and the dynamic behavior of single organisms. Therefore, developing a conceptual framework that links microbial adaptation to local environmental conditions is essential to disentangle the chemical, physiological, and ecological drivers of litter decomposition rates.

While evolution acts at the species level, our aim here is to develop a pragmatic approach for modelling complex microbial community dynamics with a minimal—albeit ecologically meaningful—set of assumptions. Furthermore, ecological and evolutionary drivers interact in regulating microbial functions by shaping community composition, motivating the study of eco-evolutionary dynamics (Loreau *et al.*, 2023; Martiny *et al.*, 2023). Models based on community-level optimality criteria have been successful in predicting scaling relations between enzyme activities and soil organic matter content at steady state (Calabrese *et al.*, 2022), as well as the relationship between microbial C-use efficiency and nutrient availability (Manzoni *et al.*, 2017). Optimal control theory has been used for investigating the temporal dynamics of decomposition (Manzoni *et al.*, 2023). However, these approaches have not yet been tested in litter decomposition models where different chemical compounds interact nonlinearly, such as in the case of lignin, which may protect high-energy compounds from decomposition by complex formation.

Optimal control theory attempts to find the optimal temporal trajectory of a model parameter (i.e. the ‘control’ variable), which maximizes a given goal function. A classic example is the partition of photosynthate into vegetative growth and reproduction with the goal of maximizing seed yield (King & Roughgarden, 1982). In this contribution, we formulated an eco-evolutionary model built on the assumption that the ligninolytic activity of the litter-decomposing community is dynamic and adapted to maximize the collective community fitness. Mathematically, this means optimizing ligninolytic activity through time to maximize the mean microbial growth rate throughout the decomposition process.

Such an optimization approach is appropriate because it allows the balancing of the costs and benefits of lignin degradation. The main benefit is access to substrates otherwise protected by the complex organic structure and complexations of lignin. The main cost is related to the maintenance of oxidative enzymes. Fungal oxidation of unhydrolysable compounds, including lignin, has been described as ‘enzymatic combustion’ (Kirk & Farrell, 1987) – an energetically costly process (Shimizu *et al.*, 2005; Moorhead *et al.*, 2013), as it relies on continuous generation of hydrogen peroxide by the fungi to be used as an electron acceptor (Mattila *et al.*, 2022). Oxidative degradation facilitates increased access to, for example cellulose and proteins, which are often protected from hydrolysis by interactions with lignin, tannins, melanin, and other unhydrolysable compounds (Berg & McClaugherty, 1987; Kirk & Farrell, 1987). It can then

be hypothesized that if oxidation is costly, it should not be initiated until ‘lignin-free’ hydrolysable compounds are depleted. Therefore, we expect our model to predict optimal lignin decomposition to start earlier in litter with initially high lignin content, or when warmer conditions promote fast microbial consumption of lignin-free compounds.

We developed and tested a minimalist model of litter decomposition that follows organic C into two pools – nonaromatic C and aromatic C. Building on the optimal control framework developed by Manzoni *et al.* (2023), we use the mean microbial growth rate as a proxy for microbial fitness to predict the optimal ligninolytic strategy. Specifically, we answer the following questions:

- (1) Does this eco-evolutionary approach have more predictive power than a model with time-invariant rate parameters?
- (2) Is climate or litter chemistry the more dominant control on ligninolytic oxidation rate?
- (3) How does the investment in ligninolytic and hydrolytic enzymes change with climate and litter chemical traits?

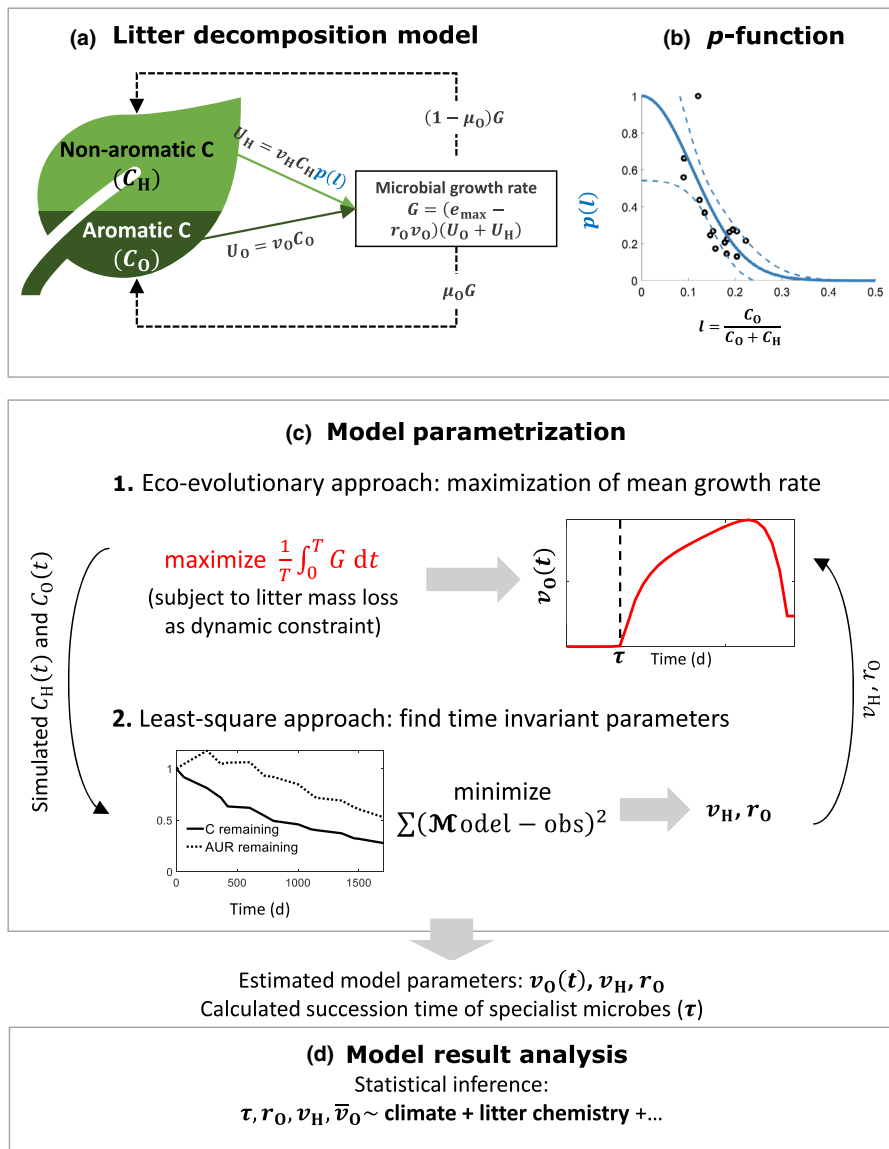
## Materials and Methods

We start by describing a two-pool litter decomposition model (Litter decomposition model section). Next, Data collation and preparation section describes the data collected from published sources used in model parametrization. The eco-evolutionary approach is described in Eco-evolutionary approach: litter decomposition as an optimal control problem section and the least-square fitting in Least-square model-data fitting section. Finally, Statistical analyses section explains the linear mixed-effect models used to identify relationships between estimated model parameters and climatic and litter chemical traits.

### Litter decomposition model

We developed a litter decomposition model that describes the interactions between litter chemistry and microbial traits. The model was parametrized using mass (or C) and lignin loss data from litter bag incubations in field conditions. ‘Lignin’ is here defined as acid unhydrolysable residues (AURs) corrected to account for measurement bias, and including both lignin and similar aromatic compounds, such as tannins and other polyphenols.

In the model, we divide litter C into a nonaromatic C pool ( $C_H$ , expressed as g of C in the modelled domain, e.g. a litter-bag), dominated by polymers susceptible to hydrolytic enzymes, including cellulose and hemicellulose, and an aromatic C pool ( $C_O$ , also expressed as g of C), representing aromatic C in lignin and condensed tannins that require oxidative ligninolytic enzymes for their decomposition (Fig. 1a). The nonaromatic pool contains both nonaromatic constituents of aromatic compounds and nonaromatic compounds that are unhydrolysable because they are complex-bound to aromatic compounds. This implies that the two pools do not decompose independently. Mathematically, the protection of nonaromatic C by aromatic C in lignocellulose complexes is simulated using a factor  $p$ , which reduces the decomposition rate of the nonaromatic pool with



**Fig. 1** Schematic of (a) litter decomposition model, (b) reduction in the hydrolytic rate ( $v_H$ ) due to the presence of aromatic carbon, as represented by the function  $p(l)$  (solid line), where  $l$  is the fraction of aromatic carbon ( $C$ ) in the litter (Eqn 1), (c) model parametrization scheme including the eco-evolutionary approach and data-model fitting, and (d) statistical inference on estimated parameters with climatic variables and litter chemical traits. Data points, obtained from Bonanomi *et al.* (2013), in (b) represent aromatic C obtained from NMR analysis, and  $p$  is the calculated (and normalized) rate of decomposition of the nonaromatic C pool. The dashed lines in panel b indicate 95% confidence interval of the scaling parameter  $a$  in Eqn 1. The succession time of specialist microbes (e.g. basidiomycete fungi) is the same as ligninolysis lag time.

increasing fraction of aromatic C (Fig. 1b). At low aromatic C contents, this protective effect is negligible, and  $p \approx 1$ ; at aromatic C contents close to 15% (on a total litter C basis), the accessibility to nonaromatic C is approximately halved.

The nonaromatic and aromatic pools are decomposed with first-order kinetics (suitable to describe dynamics at annual or longer scales), in which the rate constants account implicitly for extracellular enzyme activity. The rate constant  $v_H$  of the nonaromatic pool is time-invariant, whereas the rate constant  $v_0$  of the aromatic pool is assumed to vary through time due to dynamic changes in microbial resource acquisition strategy. For ease of interpretation, we refer to  $v_H$  and  $v_0$  as the hydrolytic and the lignolytic oxidation rate, respectively.

We assume that microorganisms can utilize both pools for growth purposes (del Cerro *et al.*, 2021); however, their C-use efficiency is at maximum ( $e_{\max}$ ) when the aromatic pool is not used and decreases linearly with increasing  $v_0$  due to metabolic

cost of producing oxidative enzymes and hydrogen peroxide to sustain oxidation (Manzoni *et al.*, 2021). The cost factor is denoted by  $r_0$  (expressed in days) and referred to as cost of ligninolytic. Furthermore, we assume a quasi-steady state for the microbial biomass so that the microbial growth rate ( $G$ ) is equal to mortality. In other words, microbial biomass is not directly modelled, but its effect on decomposition is implicitly described through the values and temporal changes in the kinetic constants. A fraction  $\mu_0$  of the microbial necromass is recycled into the aromatic pool. A higher value of  $\mu_0$  indicates that a higher fraction of microbial necromass is of aromatic nature, whereas a lower value indicates that necromass is mostly nonaromatic. With these assumptions, the mass balance equations for the nonaromatic and aromatic pools are written as,

$$\frac{dC_H}{dt} = (1 - \mu_0)G - v_H C_H p \quad \text{Eqn 1}$$

$$\frac{dC_O}{dt} = \mu_O G - v_O C_O \quad \text{Eqn 2}$$

where the microbial growth rate is given as the product of C-use efficiency (CUE, ratio of growth over C uptake) and C acquisition rate,

$$G = \text{CUE}(v_H C_H p + v_O C_O) = (e_{\max} - r_O v_O)(v_H C_H p + v_O C_O). \quad \text{Eqn 3}$$

The  $p$ -function is formulated as,

$$p = \exp\left(-\left(\frac{l}{a}\right)^2\right) \quad \text{Eqn 4}$$

where  $l = C_O/(C_O + C_H)$  and  $a$  is a scaling exponent (Fig. 1b). The energetic costs of maintaining the oxidative processes is modelled as a reduction in microbial CUE (Moorhead *et al.*, 2013; Manzoni *et al.*, 2021). Thus, CUE varies through time because of the time-dependent cost of ligninolysis, as  $\text{CUE} = e_{\max} - r_O v_O$ .

### Model parametrization

The model has six parameters:  $\mu_O$ ,  $e_{\max}$ ,  $v_O$ ,  $v_H$ ,  $r_O$  and  $a$ . The fraction of necromass C recycled into aromatic pools  $\mu_O$  was fixed based on estimates of unhydrolysable content (mainly melanin) of fungal necromass,  $\mu_O = 0.1$  (Fernandez *et al.*, 2019; See *et al.*, 2021). A few litter bag samples showed more than a doubling in unhydrolysable C from initial values, possibly due to metabolized C characterized as unhydrolysable residues in the proximate analysis. Such an increase in aromatic C is simulated by assuming a higher fraction of necromass recycled into the aromatic C pool, that is  $\mu_O = 0.3$  when fitting the model to data. The maximum growth efficiency  $e_{\max}$  was calculated as a function of the initial litter C:N ratio ( $\text{CN}_0$ ) to implicitly account for the effect of nitrogen (N) limitation of microbial growth,  $e_{\max} = \min(6.25\text{CN}_0^{-0.77}, 0.4)$  (Manzoni *et al.*, 2010). A maximum value of  $e_{\max} = 0.4$  was imposed at low  $\text{CN}_0$ . The ligninolytic oxidation rate,  $v_O$ , was estimated dynamically by maximizing the mean microbial growth rate ([Eco-evolutionary approach: litter decomposition as an optimal control problem](#) section). The hydrolytic rate,  $v_H$ , and the cost of ligninolysis,  $r_O$ , are time-invariant parameters estimated by fitting the model to the observed time series of total litter and aromatic C ([Least-square model-data fitting](#) section).

The initial mass of aromatic and nonaromatic C was directly set from the observed litter mass loss data. The initial amount of nonaromatic C (gC) was estimated by subtracting the initial amount of aromatic C (gC) from the initial total litter C (gC).

To parameterize the  $p$ -function, we utilized  $^{13}\text{C}$  NMR spectroscopy data from Bonanomi *et al.* (2013) from a litterbag incubation experiment conducted in Mediterranean and temperate environments. This NMR dataset provided information on the fraction of different functional groups within the total organic C

of the litter at four distinct time points: 0, 60, 90, and 180 d. From the NMR data, the fraction of aromatic C was determined by calculating the spectral area under the chemical shift region between 141 and 160 ppm. Since the areas under spectral regions are normalized to 1, the fraction of nonaromatic C is calculated as one minus the fraction of aromatic C. Subsequently, the fractions of aromatic and nonaromatic C were converted into amounts by multiplying them by the remaining C content within the litterbags. Utilizing the amount of nonaromatic C, we computed the first-order rate constants ( $k$ ) during the initial stage of litter mass loss, specifically within the 0–30 d period. To estimate the scaling coefficient  $a$ , we fitted a modified decay function,  $k = A \exp\left(-\left(\frac{l}{a}\right)^2\right)$ , to these  $k$  values as a function of initial fractions of aromatic C  $l$ , where  $A$  is a normalizing constant. The values of  $A$  and  $a$  are estimated using least-square fitting. Finally, the  $p$ -function is calculated as  $p(l) = \frac{k}{A} = \exp\left(-\left(\frac{l}{a}\right)^2\right)$  (Fig. 1b).

**Data collation and preparation** Litter decomposition data, encompassing total litter mass (or total C) and lignin mass (estimated as Klason lignin, acid detergent lignin, by cupric oxide (CuO) oxidation, or by near-infrared spectroscopy), were compiled from 208 published litter bag datasets from 18 studies (Table 1; Supporting Information Fig. S1). These datasets were digitized directly from the original articles or provided by the authors. Moreover, we did not include studies that indicated significant contributions of abiotic factors to the decomposition of lignin, for example via photodegradation in sites under open canopy and with intense radiation (Méndez *et al.*, 2022), because our model only simulates biotic pathways.

To ensure consistency, we treated Klason lignin, acid detergent lignin, and estimates based on near-infrared spectroscopy as AUR proxies, except for lignin reported using the CuO method (McLellan *et al.*, 1991; Berg & McClaugherty, 2014). NMR spectra have shown that AURs not only encompass most of the aromatic litter constituents, but also contain other organic compounds (Preston & Trofymow, 2015; Baskaran *et al.*, 2019). To convert AUR C into aromatic C, we used NMR spectra of AUR from *Pinus sylvestris* L. litter (Baskaran *et al.*, 2019). By fitting a linear relation between the mass of aromatic C obtained from NMR spectra and that of AUR C from proximate analysis, we determined that 20% of AUR C is aromatic (see Fig. S2). We assumed that this fraction does not change through decomposition and is the same for all litter types, allowing us to convert the time series of measured mass of AUR C to the mass of aromatic C.

Unless reported in the original sources, a 50% C content of litter and 60% C content of AUR (on a dry mass basis) were assumed (Coûteaux *et al.*, 1998; Preston & Trofymow, 2015). No conversion factor was applied to lignin reported using the CuO oxidation method. To calibrate the model to observations, we normalized litter C and aromatic C to their initial values before litterbag incubation. In line with Manzoni *et al.* (2010), for data that exhibited rapid initial C leaching (when the mass at the first measurement point decreased to less than 70% of  $C_0$ ),

**Table 1** Summary of litter decomposition datasets and estimated model parameters.

No.	Study	MAT (°C)	MAP (mm)	Initial CN (g C per gN)	Initial AUR C (g C per g total C)	$v_H$ (d <sup>-1</sup> )	$\bar{v}_O$ (d <sup>-1</sup> )	$r_O$ (d)	$\tau$ (d)	Lignin estimation method	Climate	Enzyme activity	Number of incubations
1	Berg & McLaugherty (1989)	3–8	609–799	10–147	0.12–0.50	5.0E-04–2.8E-03	2.5E-04–1.7E-03	6.5–84.2	0–608	Klason	Boreal	na	32
2	Fioritto <i>et al.</i> (2000, 2005, 2007)	19	680	46–62	0.18–0.39	9.5E-04–2.2E-03	9.9E-04–3.6E-03	1.0–17.2	0–163	Acid detergent fiber	Warm	A	3
3	He <i>et al.</i> (2016)	3	850	26–35	0.28	1.4E-03–1.9E-03	1.4E-03–1.6E-03	16.5–27.4	0–42	Acid detergent fiber	Warm	na	2
4	He <i>et al.</i> (2019)	12	2100	33–37	0.04–0.09	1.3E-03–2.9E-03	2.4E-03–4.8E-03	3.3–27.0	0	CuO oxidation	Warm	na	4
5	Hirobe <i>et al.</i> (2004)	26	3850	40–73	0.35–0.62	3.1E-03–1.0E-02	1.8E-03–1.2E-02	0.6–26.3	0–12	Klason	Temperate	na	15
6	Huang <i>et al.</i> (2021)	20	1200	29	0.22	2.4E-03–3.7E-03	3.9E-04–2.2E-03	12.9–26.8	93–208	Acid detergent fiber	Tropical	A	4
7	Kou <i>et al.</i> (2015)	18	1475	36–69	0.18–0.26	1.3E-03–2.1E-03	2.1E-04–6.9E-04	13.5–42.0	124–389	Klason	Warm	na	9
8	Magill & Aber (1998)	4	1120	42–78	0.20–0.49	5.0E-04–1.5E-03	2.2E-04–1.3E-03	9.8–83.9	0–815	Near-infrared spectroscopy	Temperate	na	18
9	McKee <i>et al.</i> (2016)	13	835	30	0.01	2.1E-03	4.3E-03	1.6	123	Acid detergent fiber	Cool	na	1
10	Osono (2017)	21	2487	20–110	0.32–0.55	2.1E-03–6.0E-03	8.8E-04–6.8E-03	1.5–36.3	0–232	Klason	Warm	na	12
11	Osono & Takeda (2005)	10	2495	17–95	0.60	9.6E-04–5.0E-03	5.0E-04–7.2E-03	1.0–113.1	0–203	Klason	Temperate	na	28
12	Preston <i>et al.</i> (2009a,b)	–3 to 7	370–1258	45–1379	0.22–0.51	4.4E-04–1.7E-03	2.1E-04–1.3E-03	7.1–129.0	0–1029	Klason	Cool	na	15
13	Růžek <i>et al.</i> (2021)	6	1000	53	0.04	1.6E-03–1.8E-03	1.8E-03–2.2E-03	6.5–7.7	0–60	CuO oxidation	Cool	na	4
14	Šnajdr <i>et al.</i> (2011)	9	647	49	0.49	4.0E-03	2.5E-03	12.7	22	Klason	Temperate	A	1
15	Tu <i>et al.</i> (2011)	16	1490	90–137	0.22–0.32	1.2E-03–4.0E-03	1.4E-03–7.1E-03	0.5–5.9	0–113	Acid detergent fiber	Warm	na	12
16	Tu <i>et al.</i> (2014)	16	1822	20–265	0.18–0.46	1.4E-03–6.9E-03	1.4E-03–1.2E-02	0.5–16.3	0–140	Acid detergent fiber	Warm	na	40
17	Yue <i>et al.</i> (2016)	3	850	13–60	0.37–0.60	2.8E-03–1.1E-02	1.1E-03–1.3E-02	2.4–29.1	0–67	Acid detergent fiber	Temperate	na	4
18	Zhou <i>et al.</i> (2017)	16	1772	52	0.22	2.9E-03–3.7E-03	1.5E-03–2.9E-03	9.2–19.4	138–216	Acid detergent fiber	Warm	na	4

$\bar{v}_O$ , mean rate constant of aromatic pool;  $r_O$ , cost of ligninolytic enzyme production;  $v_H$ , rate constant of nonaromatic pool; A, enzyme activity available; CN, C-to-N ratio; MAP, mean annual precipitation; MAT, mean annual temperature; na, enzyme activity not available;  $\tau$ , lag time of ligninolytic enzyme, Number of incubations are the observations available. One set of observations is total C and AUR loss time series data.



the initial data point was excluded. Furthermore, we applied a  $(C_t - C_{t-1})/C_{t-1} > 0.1$  threshold to remove data points that implied increases in litter mass possibly caused by contamination from external sources.

**Eco-evolutionary approach: litter decomposition as an optimal control problem** Following Manzoni *et al.* (2023), we formulated litter decomposition as an optimal control problem where we assumed that the microbial community maximizes its mean growth rate over the entire decomposition period ( $T$ ) by adapting ligninolytic oxidation. The maximization objective ( $J$ ) can be written as,

$$J = \frac{1}{T} \int_0^T G dt \quad \text{Eqn 5}$$

This maximization is constrained by the mass balance Eqns 1 and 2 and constitutes a fixed terminal time and free terminal state problem (Lenhart & Workman, 2007). In other words, the outcome of this optimization problem is an optimal variation in  $v_O$  that maximizes microbial growth rate in the specified period of time  $T$  for a given initial litter chemistry (Fig. 1c).

In principle, the period during which microorganisms maximize their growth can also be optimized. These problems are referred to as free terminal time problems in the literature on optimal control and are numerically more challenging to solve. To keep the problem numerically tractable, we defined the decomposition period as the time when half the mass remaining at the last litter bag harvest was attained. This time was calculated by fitting a single exponential model to litter mass loss data. This procedure only provides the terminal time for the optimization and does not imply that the modelled decomposition trajectories are exponential.

The optimal control problem was solved with numerical methods based on direct collocation, using the Yop toolbox in MATLAB (Leek, 2016).

**Least-square model-data fitting** We determined the time-invariant parameters  $v_H$  and  $r_O$  by least-square fitting of the model output to the time series of total litter C and aromatic C (Fig. 1c). Briefly, we initialized the least-square solver with a guess of  $v_H$  and  $r_O$  and then ran the optimal control problem to obtain an estimate of the optimal  $v_O$  and the temporal dynamics of the state variables  $C_H$  and  $C_O$ . The optimal  $v_O$  was recalculated at each iteration of the least-square solver. Subsequently, we compared the sum of  $C_H$  and  $C_O$  with the measured total litter C, and  $C_O$  with the measured aromatic C using a mean square error metric. To obtain the best-fitted parameters for each litter bag dataset, we employed the MATLAB *lsqcurvefit* function. We used the coefficient of determination ( $r^2$ ) and the root mean squared error (rmse) to evaluate model performance.

Additionally, for comparison with the optimally controlled  $v_O$  model, we also fitted the same model (Eqns 1, 2) to the same data but with time-invariant  $v_O$ . This simpler model version is formally similar to conventional litter decomposition (or soil C)

models with fixed parameters. Finally, using a Bayesian information criterion, we compared the predictive accuracy of these two models.

## Statistical analyses

Using the best-fitted parameters, we estimated the ligninolysis lag time ( $\tau$ ) as the time when  $v_O$  increased above 5% of the maximum value (i.e. at the threshold  $v_O > 0.05 \max(v_O)$ ). This lag time was used as an index to characterize the timing of aromatic C degradation, while the temporal average of ligninolytic oxidation rate  $\bar{v}_O$  and the peak value of  $v_O$  (calculated as  $\max(v_O)$ ) were used as indices of the aromatic C decomposition capacity.

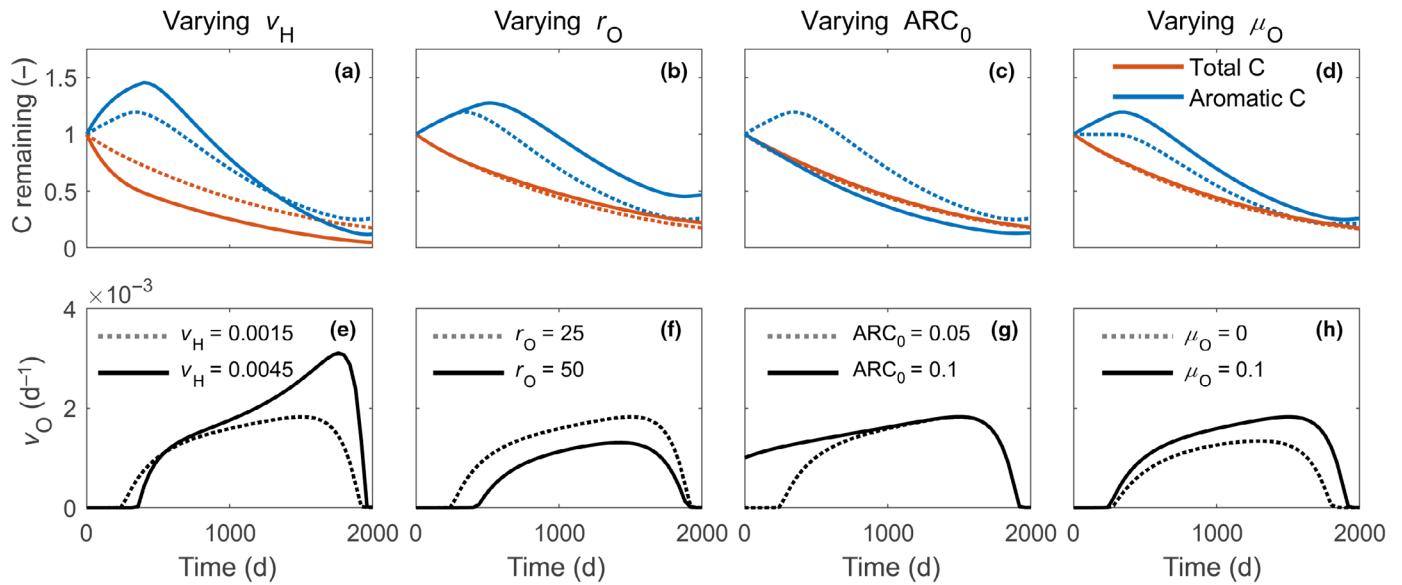
We used linear mixed-effect models to disentangle the effects of climate and litter chemistry on aromatic C and litter decomposition rates. These models treated  $\tau$ ,  $v_H$ ,  $r_O$ ,  $\max(v_O)$ , and  $\bar{v}_O$  as response variables. The predictor variables were mean annual temperature (MAT), mean annual precipitation (MAP), initial litter C:N ratio ( $CN_0$ ), initial aromatic C to litter N ratio, and the initial aromatic C. In the final model, we only used MAT,  $CN_0$ , and initial aromatic C to reduce collinearity among predictors. To enhance interpretability, all predictors were centered and scaled. Additionally, the data source was included as a random effect on the intercept to account for any study-specific variation. The  $Q_{10}$  temperature sensitivity values for hydrolytic and ligninolytic oxidation rates were estimated using fixed effect sizes of MAT from the linear mixed-effect model, and nonparametric bootstrapping was used to calculate confidence intervals.

All response variables were log-transformed to ensure the normality of residuals. Notably, the lag time  $\tau$  exhibited a zero-inflated response. Therefore, we transformed it using  $\log(\tau + K)$ , where  $K = 0.5 \min(\tau > 0)$  was introduced to address instances where  $\tau$  equaled zero. We also fitted  $\tau$  using a zero-inflated generalized linear model from *glmmTMB* (Brooks *et al.*, 2017). However, here we only present results from the linear mixed-effect model because both resulted in similar significance levels for the predictors, and it is more straightforward to interpret coefficient estimates in linear models. The MATLAB *fitlme* function was used to perform these analyses.

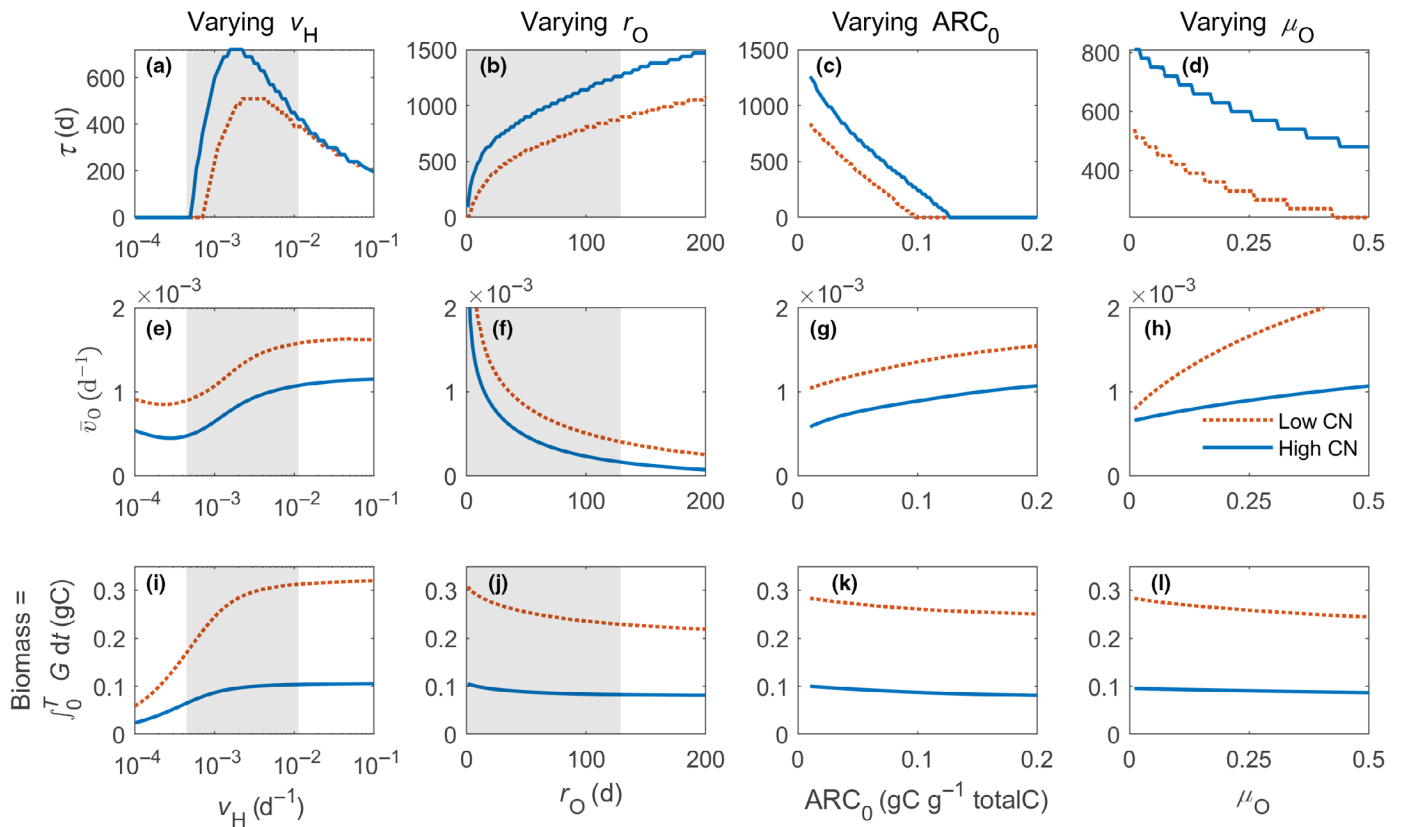
## Results

We start by presenting numerical explorations of model behavior (Figs 2, 3), followed by examples of model fitting (Fig. 4), model performance metrics (Fig. 5), and the results from the statistical analysis of how litter chemistry and climate affect model parameters (Figs 6, 7).

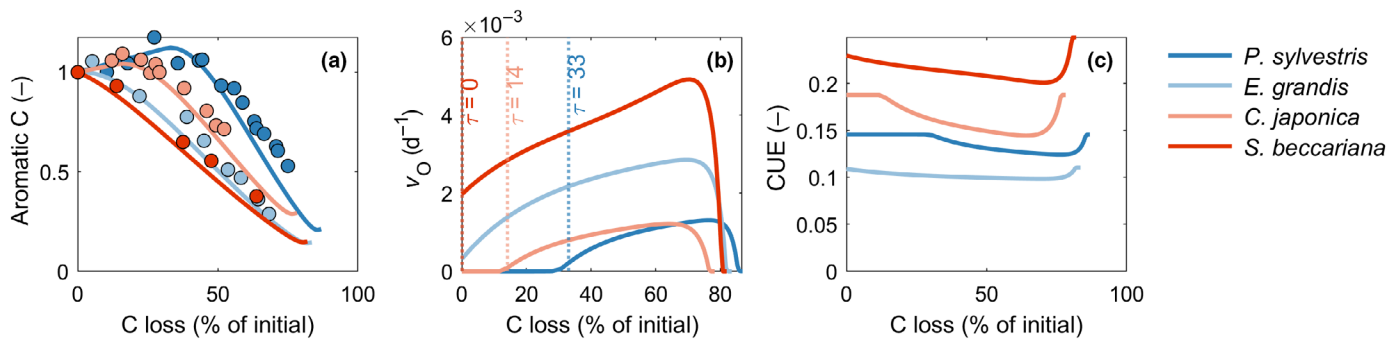
The first numerical exploration illustrates the temporal changes in total C remaining (red curves), aromatic C remaining (blue curves), and the optimal ligninolytic oxidation rate  $v_O$  (black curves) for different values of the time-invariant parameters hydrolytic rate  $v_H$ , cost of ligninolysis  $r_O$ , initial aromatic C, and necromass recycling into the aromatic C pool  $\mu_O$  (Fig. 2). Our optimization approach predicted a temporally variable ligninolytic oxidation rate  $v_O$ . The optimal  $v_O$  was initially zero, but after a lag, it increased steeply, attained a maximum in the



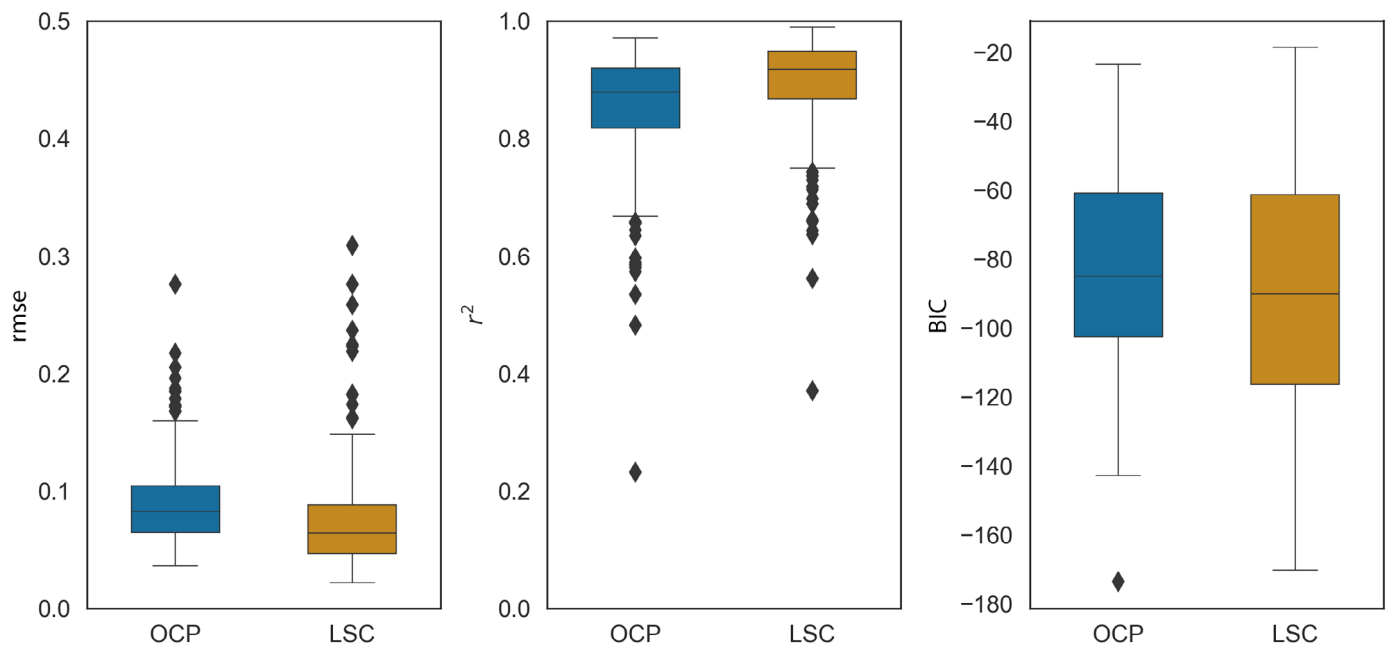
**Fig. 2** Effect of the hydrolytic rate ( $v_H$ ), cost of ligninolysis ( $r_O$ ), initial fraction of aromatic C ( $ARC_0$ ), and necromass cycling into the aromatic carbon (C) pool ( $\mu_O$ ) on (a–d) total litter C remaining and the aromatic C pool remaining, and (e–h) ligninolytic oxidation rate ( $v_O$ ). Both C pools are expressed relative to the initial amounts. The dashed or solid lines denote low or high levels of the parameters being varied. Values of the fixed parameters in simulations are:  $v_H = 0.0015 \text{ d}^{-1}$ ,  $r_O = 25 \text{ d}$ ,  $\mu_O = 0.1$ ,  $CN_0 = 50$ , and  $ARC_0 = 0.05$ .



**Fig. 3** Effect of the hydrolytic rate ( $v_H$ ), cost of ligninolysis ( $r_O$ ), initial fraction of aromatic carbon (C) ( $ARC_0$ ), and necromass cycling into the aromatic C pool ( $\mu_O$ ) on (a–d) lag time of ligninolysis ( $\tau$ ), (e–h) temporal average of the ligninolytic oxidation rate ( $\bar{v}_O$ ), and (i–l) cumulative microbial biomass growth. Values of the fixed parameters are:  $v_H = 0.0015 \text{ d}^{-1}$ ,  $r_O = 25 \text{ d}$ ,  $ARC_0 = 0.05 \text{ gC g}^{-1} \text{ litter}$ , and  $\mu_O = 0.1$ . Red and blue lines represent low initial litter C : N ratio = 20 and high C : N ratio = 100, respectively. Mean rates are calculated from a fixed simulation period of 2000 d. The grey patch areas represent the observed range of estimated  $v_H$  and  $r_O$ .



**Fig. 4** Examples of model fitting: variation in (a) amount of aromatic carbon (C) normalized by the initial value, (b) lignolytic oxidation rate ( $v_O$ ), and (c) C-use efficiency, as a function of total C loss. Solid symbols represent observed ARC and total C loss measured at the same time points. Four litter types with contrasting initial aromatic C and initial C : N ratio from four different climates were chosen as examples—boreal: *Pinus sylvestris* L. leaves,  $ARC_0 = 0.04$ ,  $CN_0 = 132$ ,  $r^2 = 0.96$ ,  $rmse = 0.05$  from Berg & McClaugherty (1989), cold temperate: *Cryptomeria japonica* D. leaves,  $ARC_0 = 0.08$ ,  $CN_0 = 95$ ,  $r^2 = 0.97$ ,  $rmse = 0.03$  from Osono & Takeda (2005), warm temperate: *Eucalyptus grandis* H. twigs  $ARC_0 = 0.06$ ,  $CN_0 = 189$ ,  $r^2 = 0.98$ ,  $rmse = 0.03$  from Tu *et al.* (2014), and tropical: *Shorea beccariana* B. leaves,  $ARC_0 = 0.1$ ,  $CN_0 = 66$ ,  $r^2 = 0.98$ ,  $rmse = 0.03$  from Hirobe *et al.* (2004). Ligninolysis lag time ( $\tau$ ) values are in days.



**Fig. 5** Comparison of root mean squared error ( $rmse$ ), coefficient of determination ( $r^2$ ), and Bayesian information criterion (BIC) between optimal control model (OCP) and least-square fitting model (LSC). The ends of each box represent the 25<sup>th</sup> and 75<sup>th</sup> quantiles of  $rmse$ ,  $r^2$ , and BIC, and the horizontal line within the box represents the median. Whiskers of each boxplot extend from the minimum and maximum values in 1.5 times interquartile range. Diamond points are outliers falling outside the whisker range.

intermediate phase of decomposition, and then decreased as the amount of C in both pools decreased. Increasing the hydrolytic rate  $v_H$  or the cost of ligninolysis  $r_O$  delayed decomposition of aromatic C, whereas increasing initial aromatic C or necromass recycling into the aromatic C pool  $\mu_O$  reduced the lag time of ligninolysis. The lag time was most sensitive to initial aromatic C – a chemical trait that emerged as a key predictor also in the following analysis. A direct consequence of this temporal variation in optimal  $v_O$  is that the aromatic C can accumulate initially before ligninolysis starts or remain constant when  $v_O$  begins to increase but necromass recycling balances aromatic C decomposition.

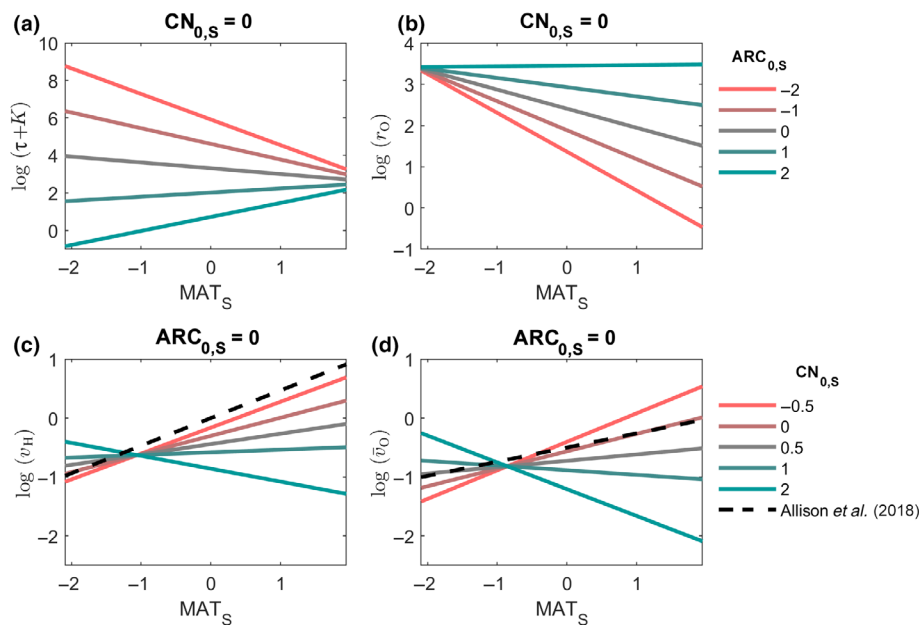
Aromatic C eventually decreases with rates similar to the whole litter C when  $v_O$  is sufficiently high (blue curves in Fig. 2). These different phases of the aromatic C trajectory vary not only according to  $v_O$ , but also depending on other model parameters.

Fig. 3 shows variation in three metrics that summarize the whole decomposition process: lag time of ligninolysis ( $\tau$ , top row), temporal average of lignolytic oxidation rate ( $\bar{v}_O$ , middle row), and cumulative microbial biomass growth (bottom row), as a function of other, time-invariant model parameters. As the rate of hydrolysis  $v_H$  was increased, the lag time remained close to zero for very low values of  $v_H$  and then peaked at intermediate



$\log(\tau+K)$	$-0.31 \pm 0.32$ ns	$-0.088 \pm 0.13$ ns	$-1.3 \pm 0.13$ ***	$-0.013 \pm 0.22$ ns	$0.53 \pm 0.12$ ***	$-0.69 \pm 0.27$ *	(0.31, 0.79)
$\log(r_O)$	$-0.46 \pm 0.22$ *	$-0.045 \pm 0.093$ ns	$0.52 \pm 0.097$ ***	$0.14 \pm 0.16$ ns	$0.24 \pm 0.089$ **	$-0.21 \pm 0.2$ ns	(0.23, 0.74)
$\log(v_H)$	$0.31 \pm 0.095$ **	$-0.28 \pm 0.037$ ***	$-0.16 \pm 0.039$ ***	$-0.26 \pm 0.064$ ***	$0.052 \pm 0.036$ ns	$0.023 \pm 0.078$ ns	(0.37, 0.82)
$\log(\bar{v}_O)$	$0.3 \pm 0.17$ .	$-0.32 \pm 0.063$ ***	$-0.11 \pm 0.067$ .	$-0.38 \pm 0.11$ ***	$-0.13 \pm 0.061$ *	$0.15 \pm 0.13$ ns	(0.13, 0.78)
$\log(\max(v_O))$	$0.39 \pm 0.16$ *	$-0.47 \pm 0.065$ ***	$-0.3 \pm 0.068$ ***	$-0.45 \pm 0.11$ ***	$-0.1 \pm 0.062$ ns	$0.25 \pm 0.14$ .	(0.3, 0.76)
	$MAT_S$	$CN_{0,S}$	$ARC_{0,S}$	$MAT_S \times CN_{0,S}$	$MAT_S \times ARC_{0,S}$	$CN_{0,S} \times ARC_{0,S}$	$(r_{\text{marg}}^2, r_{\text{cond}}^2)$

**Fig. 6** Estimates of fixed effects and their SE from linear mixed-effect models to predict ligninolysis lag time  $\log(\tau + K)$ , cost of ligninolysis  $\log(r_O)$ , the hydrolysis rate  $\log(v_H)$ , and temporal average and maximum of the ligninolytic oxidation rate, respectively  $\log(\bar{v}_O)$ ,  $\log(\max(v_O))$ , as a function of mean annual temperature ( $MAT_S$ ), initial C : N ratio ( $CN_{0,S}$ ), initial fraction of aromatic carbon (C) ( $ARC_{0,S}$ ), and their interaction terms as predictors. Red represents a negative relationship between response and predictor, green represents a positive relationship, and white represents an insignificant estimate. The rightmost column describes the marginal ( $r_{\text{marg}}^2$ ) and conditional ( $r_{\text{cond}}^2$ ) coefficients of determination. Subscript 'S' denotes that the predictors are scaled and centered to mean 0 and SD 1. Star symbols denote significance levels: \*\*\*,  $P < 0.001$ ; \*\*,  $P < 0.01$ ; \*,  $P < 0.05$ ; .,  $P < 0.1$ , ns as not significant  $P > 0.1$ .



**Fig. 7** Simulated variation of (a) ligninolysis lag time  $\log(\tau + K)$ , (b) cost of ligninolysis  $\log(r_O)$ , (c) hydrolysis rate  $\log(v_H)$ , and (d) temporal average ligninolytic oxidation rate  $\log(\bar{v}_O)$  with changing mean annual temperature ( $MAT_S$ ), initial C:N ratio ( $CN_{0,S}$ ), and initial fraction of aromatic carbon (C) ( $ARC_{0,S}$ ) using only the fixed effects from linear mixed-effect models. Note that for  $\log(v_H)$  and  $\log(\bar{v}_O)$  lines with different colors show variation with changing  $CN_{0,S}$  and fixed  $ARC_{0,S} = 0$ , while for  $\log(\tau + K)$  and  $\log(r_O)$  lines with different colors show variation with changing  $ARC_{0,S}$  and fixed  $CN_{0,S} = 0$ . Subscript 'S' denotes that the predictors are scaled and centered to have mean = 0 and SD = 1. The black dashed line in panels (c) and (d) denotes the average temperature sensitivity observed for hydrolytic and ligninolytic enzymes by Allison et al. (2018).

values of  $v_H$  (Fig. 3a). This implies that the decomposition of the aromatic C started immediately if the decomposition of nonaromatic C was not favorable (low values of  $v_H \approx 1E-4$  d<sup>-1</sup>), resulting in a nonzero value of  $\bar{v}_O$  (Fig. 3c). As the decomposition of nonaromatic pools became faster (increasing values of  $v_H$ , in the range of  $1E-4$  to  $3E-4$  d<sup>-1</sup>), the rate of decomposition of the aromatic C was slightly reduced, but the lag time remained close to zero. However, for higher values of  $v_H > 3E-4$  d<sup>-1</sup>, increasing  $v_H$  increased the  $\bar{v}_O$  with a significant increase in lag time. For very high values of  $v_H > 1E-2$  d<sup>-1</sup>,  $\bar{v}_O$  remained stable.

Increasing the cost of ligninolysis  $r_O$  increased the lag time (Fig. 3b), while increasing initial aromatic C decreased it

(Fig. 3c). Above a threshold of initial aromatic C  $c$ : 0.1 g aromatic C/g litter C, the lag time decreased to zero. Furthermore, increasing the fraction of necromass recycling into the aromatic C pool decreased the lag time (Fig. 3d) because having more C in the aromatic pool promotes its decomposition. Variation in average ligninolysis rate  $\bar{v}_O$  followed opposite trends compared with lag time when increasing  $r_O$ ,  $ARC_{0,S}$ , or  $\mu_O$  (Fig. 3f–h).

The cumulative microbial biomass growth increased with increasing hydrolytic rate  $v_H$ , and decreased with increasing cost of ligninolysis  $r_O$ , initial aromatic C and necromass recycling into the aromatic C pool  $\mu_O$ , although variations due to the last two factors were minor (Fig. 3i–l). These trends can be explained

by the positive effect of nonaromatic C acquisition on growth, the negative effect of enzyme costs and litter recalcitrance, and the negative effect of recycling necromass in the aromatic C pool.

All metrics shown in Fig. 3 also depended on the initial litter C : N ratio (blue vs orange curves in Fig. 3), which was implemented via CUE in our model. A lower value of  $CN_0$  implies lower N limitation, thus higher CUE and growth rate (dashed curves are all higher than the solid curves in Fig. 3i–l). Ultimately, higher CUE caused a larger fraction of decomposed C to be recycled as necromass, stimulating the decomposition of aromatic C (Fig. 3e–h) and decreasing lag time (Fig. 3a–d). Therefore, the effects of initial litter  $CN_0$  on decomposition are all mediated by the feedback of CUE and growth on the dynamics of aromatic C.

In Fig. 4(a), four examples of least-square fitting of the model to total C and aromatic C loss data are shown. The selected data sets span different climates and initial litter quality to illustrate the range of behaviors in the data (and model output). The optimal ligninolytic oxidation rate  $v_O$  showed a similar pattern as in Fig. 2(e–h), with a peak of ligninolytic enzyme activity during late stages of decomposition, at c. 60–80% C loss (Fig. 4b). The estimated lag time was lowest ( $\tau = 0$ ) in the *Shorea beccariana* litter, which had the highest initial aromatic C among the four litters; lag time was most delayed in the *Pinus sylvestris* litter, which had the lowest initial aromatic C (Fig. 4b). Furthermore, the CUE was lower in litter with higher  $CN_0$ , and decreased as decomposition proceeded because of ligninolysis costs (Fig. 4c). These examples are representative of the typical model performance, which was overall good, with  $r^2$  generally higher than 0.8 and rmse lower than 0.1 g C/g initial C (Fig. 5). Notably, the two model variants – optimized  $v_O$  vs time-invariant  $v_O$  – performed similarly well (Fig. 5).

The results of the linear mixed-effect model used to identify the drivers of model parameters are shown in Fig. 6 (see also Figs S3, S4, S5; Table S1). The lag time of ligninolysis decreased with increasing initial aromatic C regardless of climate (Fig. 7a). It also decreased in warmer climates at low initial aromatic C, but increased in warmer climates at high initial aromatic C (Fig. 7a). The cost of ligninolysis  $r_O$  increased with increasing initial aromatic C and decreased in warmer climates, though temperature effects were most apparent at low initial aromatic C (Fig. 7b). The hydrolytic rate  $v_H$  increased in warmer conditions for low values of  $CN_0$ , but decreased for high  $CN_0$  (Fig. 7c). The temporal average of the ligninolytic oxidation rate  $\bar{v}_O$  followed the same patterns as  $v_H$  (Fig. 7d).

To compare the temperature sensitivities of hydrolytic and ligninolytic oxidation rates to observations, we used  $Q_{10}$  values reported by Allison *et al.* (2018). The temperature sensitivities of both  $v_H$  and  $\bar{v}_O$  at low  $CN_0$  were closer to the observed temperature sensitivities of hydrolytic and oxidative enzymes, respectively (black dashed lines in Fig. 7c,d). The  $Q_{10}$  values of the maximum ligninolytic oxidation ( $1.72 \pm 0.16$ ) rate were significantly higher than those of hydrolytic decomposition ( $1.53 \pm 0.11$ ) and the temporal average of ligninolytic oxidation ( $1.47 \pm 0.26$ ; Fig. S6). Furthermore, the  $Q_{10}$  of hydrolytic decomposition was significantly higher than the  $Q_{10}$  of the temporal average of ligninolytic oxidation (Tables S2, S3).

## Discussion

Our litter decomposition model is based on an eco-evolutionary approach, assuming that ligninolysis is regulated to maximize the fitness of the microbial community. Using this model, we elucidated the effect of climate and litter quality on the decomposition rates of aromatic (lignin and other phenolics) and nonaromatic C compounds (soluble, cellulose, hemicellulose, proteins, and lipids). Here, we start discussing these results from a methodological perspective (Eco-evolutionary approach vs model with time-invariant rate parameters section); next, we focus on the patterns of ligninolytic oxidation (Simulated temporal patterns in optimal ligninolytic activity section); then, the chemical and climatic drivers are considered (Climate and litter quality controls ligninolysis section), and finally, a broad discussion on the application of eco-evolutionary principles in C cycling models is provided (Eco-evolutionary dynamics in carbon cycling models section).

### Eco-evolutionary approach vs model with time-invariant rate parameters

Optimization approaches, such as the one proposed here, could help reduce the degrees of freedom (and related equifinality issues) of current, often over-parameterized models (Marschmann *et al.*, 2019; Harrison *et al.*, 2021). If optimization provides time-dependent model parameters, it can also capture the consequences of dynamic changes, such as alterations in enzyme production resulting from changes in microbial community composition as decomposition progresses. This possibility motivated our first question: whether the optimization model has higher predictive power than an alternate model with a time-invariant ligninolytic oxidation rate. We found that both models performed well, and their BIC values were similar, even though the model with time-invariant parameters has three fitting parameters and the optimization model has only two (Fig. 5). This indicates that the eco-evolutionary approach – substituting an unconstrained parameter with a maximization criterion (Eqn 5) – has equivalent performance as the more traditional model. This result is encouraging, as the optimization approach provides a framework informed by ecological theory that includes tradeoffs among microbial traits (here, ligninolytic capacity and C-use efficiency) and predicts temporal trait variation without requiring new observations for parametrization.

### Simulated temporal patterns in optimal ligninolytic activity

Decomposition of the aromatic C pool increases the accessibility of protected cellulose and proteins, but low-molecular size products of complex aromatic polymers, such as lignin, can also actively enter metabolism to support microbial growth (del Cerro *et al.*, 2021). As a result, investment in ligninolytic enzymes might yield dual benefits. While some microbial explicit litter decomposition models have explored the effects of lignin-mediated carbohydrate protection on uptake rates and microbial C-use efficiency (Moorhead & Sinsabaugh, 2006; Manzoni *et al.*, 2021), none have investigated the emergent ligninolytic capacity

that arises from maximizing cumulative growth rate. Our model capitalizes on the dual influences of the aromatic C pool, enabling us to predict optimal temporal variation in ligninolytic oxidation ( $v_O$ ) during litter decay (Fig. 2).

Since  $v_O$  serves as a proxy for overall ligninolytic enzyme activity, a direct comparison with observed enzyme activities (e.g. peroxidase, laccase, or polyphenol oxidase) is not straightforward, because ligninolytic enzymes are multifaceted (Sinsabaugh, 2010) and several enzymes may act together to decompose aromatic compounds (Mori *et al.*, 2023; Schimmel, 2023). Despite these methodological limitations, the simulated pattern of  $v_O$  was qualitatively similar to the activities of peroxidase and laccase enzymes reported in Huang *et al.* (2021) and Šnajdr *et al.* (2011; Fig. S7). The only notable difference between observations and model results was in the dataset by Huang *et al.* (2021), in which enzyme activity exhibited an early peak that our model could not predict. Such a peak is difficult to explain but is consistent with the early loss of lignin in that particular dataset. Overall, this independent evidence based on measured enzymatic activities lends additional support for the predicted decomposition patterns in the aromatic C pool.

Patterns in ligninolytic oxidation rate are explained by the controls of hydrolytic decomposition, cost of ligninolysis, and initial aromatic C, as these parameters combine the effects of climate, microbial metabolic tradeoff, and litter chemistry (Fig. 3). Depending on these parameters, the microbial community may initiate production of ligninolytic enzymes already in early stages of litter decay, or there might be a more or less long lag in ligninolytic activity leading to the often observed initial accumulation of aromatic C (Cotrufo *et al.*, 2015; Barbi *et al.*, 2020). When litter has a higher initial content of aromatic C, microorganisms prioritize the removal of the aromatic C to access the nonaromatic C, resulting in higher optimal rates of ligninolytic oxidation  $v_O$  and reduced lag time (Fig. 3c,g). However, microorganisms with a lower cost of ligninolysis, leading to higher CUE, can achieve higher growth rates, thereby facilitating increased investment in ligninolytic enzymes and subsequently increasing  $v_O$  (Fig. 3b,f). Notably, as the cost of ligninolysis is reduced, the initial aromatic C threshold level at which the lag time becomes zero is also lower (as illustrated in Fig. S8).

From the estimated parameters, we found a positive relation between hydrolytic and mean ligninolytic oxidation rates (see  $\log(v_H)$  vs  $\log(\bar{v}_O)$  in Fig. S3; the range of these parameters is also illustrated as shaded areas in Fig. 3) – implying that faster hydrolysis is linked to faster ligninolysis. This coordination is particularly relevant in tropical forests, where warm and humid conditions prompt swift losses of labile litter pools, which in turn can increase losses of the more recalcitrant litter pool, thereby reducing the aromatic contribution to stable soil C. On the contrary, in cold climates and N-limited conditions, slow hydrolysis may lead to delayed aromatic C oxidation and accumulation of recalcitrant, aromatic residues. However, when hydrolytic C acquisition is very rapid (high  $v_H$ ) or very slow (low  $v_H$ ), the cumulative growth rate can only increase through decomposition of the aromatic pool, necessitating an early increase in  $v_O$  (i.e. short lag time; see Fig. 3a,e). In reality, forcing low  $v_H$  as we did

in the numerical analysis of Fig. 3 might not be realistic, because hydrolytic enzymes are produced together with oxidative enzymes. High  $v_H$  is more likely to occur, and in that case it is reasonable to expect – as predicted by the model and estimated parameters – that ligninolytic capacity would also increase and start earlier during decomposition.

### Climate and litter quality controls ligninolysis

We found that the lag time ( $\tau$ ) decreased, even though the predicted cost of ligninolysis ( $r_O$ ) increased, with increasing initial aromatic C under all climatic conditions (red to green lines, Fig. 7a, b). This implies that microorganisms decomposing litter with higher initial aromatic C will invest early in ligninolytic enzymes because the benefits of accessing nonaromatic C outweigh the costs of ligninolysis. Furthermore, this effect was enhanced for N-poor litter (significant negative  $ARC_0 \times CN_0$  term for  $\tau$  in Fig. 6). By contrast, the average ligninolytic oxidation rate decreased at a higher initial C:N ratio, indicating that the average rate of aromatic C decomposition is slower in N-poor litter, consistent with findings by Talbot & Treseder (2012), who reported a decrease in lignin decay rate as litter C:N increased. Theoretically, in N-poor litter, decomposers may benefit if oxidation of aromatic litter components releases growth-limiting substrates, for example from protein–tannin complexes. Such mining for tightly bound N may be suppressed in N-rich litter (Craine *et al.*, 2007). Taken together, these results support the traditional hypothesis that microorganisms consume easily degradable C during the early stages of litter decay and later co-metabolize lignocellulose to access C and N from protected sugars and proteins (Berg & Staaf, 1980).

The effect of increasing temperature on lag time depended on initial aromatic C. The lag time decreased in warmer climates for high-quality litter (low initial aromatic C) but increased for low-quality litter (high initial aromatic C) due to the decreasing cost of ligninolysis with increasing temperature.

This study only included data on MAT, initial litter C:N ratio, and initial proportion of aromatic C, which explained 10–40% of the variance of the response variables. Other studies have reported that soil pH, fungal diversity and community composition, fungi-to-bacteria ratio, and soil minerals (e.g. Mn, Fe) correlate with aromatic C decomposition rates (Huang *et al.*, 2023). Here, we assumed that the effects of these potential predictors (for which we do not have complete data) are captured by including the data source as a random factor (which accounted for an additional 40–60% of the variance of the response variables, Table S1). In addition, our model does not account for microbial adaptation under conditions of N limitation or N excess, which could affect the relationship between ligninolytic oxidation and the C:N ratio of litter. We leave the development of such a model for a future contribution.

Warming accelerates microbial metabolism, but the sensitivity of decomposition rates to temperature also depends on other factors, such as substrate quantity and quality (Davidson & Janssens, 2006). We found that climate (MAT) and initial litter quality (initial aromatic C and C:N) together controlled the rates of hydrolysis ( $v_H$ ) and ligninolytic oxidation ( $\bar{v}_O$ ) and

max( $v_0$ ). The  $Q_{10}$  value of hydrolysis was higher than that of average ligninolytic oxidation, as also shown in empirical studies in litter (Nottingham *et al.*, 2016; Allison *et al.*, 2018; Tan *et al.*, 2020). However, the  $Q_{10}$  of maximum ligninolytic oxidation was even higher, suggesting that ligninolytic enzymes exhibit varying temperature sensitivity at different stages of litter decay (e.g. Duboc *et al.*, 2014). In soils, ligninolytic enzymes can have higher  $Q_{10}$  than hydrolytic enzymes (Davidson & Janssens, 2006; Wetterstedt *et al.*, 2010; Wang *et al.*, 2012), consistent with our results for maximum ligninolytic oxidation rate (Fig. 7).

### Eco-evolutionary dynamics in carbon cycling models

The microbial engine that drives recycling of C and nutrients continuously adapts to the local conditions. For microbial systems, the evolutionary time scale is intermingled with ecological processes (changes in community composition), giving rise to eco-evolutionary dynamics at the community scale (Loreau *et al.*, 2023; Martiny *et al.*, 2023). These eco-evolutionary dynamics can feedback on soil C cycling in ways that are still not fully explored (Abs *et al.*, 2022). Here, we found wide ranges of estimated hydrolytic rates, cost of ligninolysis, and of the optimized temporal variation in ligninolytic oxidation rates, making a strong case against using fixed values of these parameters in soil and ecosystem models. Therefore, developing a framework accounting for adaptation of microbial resource acquisition strategies in a tractable manner that can be upscaled and integrated into a large-scale model is a much-needed advancement.

One major challenge in modelling microbial adaptation is the mathematical representation of eco-evolutionary dynamics governing the variation in parameters reflecting the plasticity of microbial functional traits in individual taxa, or the breadth of community composition variations driving community-level trait variation. Recent literature has proposed various mathematical approaches that employ optimality principles to elucidate optimal tradeoffs in organism life-history traits, thereby establishing a link between eco-evolutionary dynamics and shifting environmental conditions. For example, using an adaptive dynamics framework, Abs *et al.* (2022) showed that when tradeoffs between growth and extracellular enzyme production are accounted for, estimated losses of global C stocks increase. A simpler optimal control approach by Manzoni *et al.* (2023) showed that the optimal foraging strategy that maximizes microbial growth rate in a competitive environment favors high rates of resource uptake and low growth efficiency. These principles, rooted in optimizing resource allocation, extend beyond microbial systems and have been applied to plants (Feng *et al.*, 2022; Bassiouni *et al.*, 2023), underscoring their potential generality across diverse ecological contexts.

### Conclusion

We developed a novel litter decomposition model based on an eco-evolutionary approach that maximizes mean microbial growth rate by finding the optimal ligninolytic activity. This model, constrained by >200 litter mass loss datasets, was used to assess the rate and starting time of decomposition of aromatic C (i.e. lignin and other

phenolics) in plant litter. Climate and litter chemical quality interacted in controlling aromatic C decomposition. Specifically, warmer conditions accelerated decomposition rates, shortened the lag time of ligninolytic enzyme expression, and enhanced microbial C-use efficiency by reducing the predicted costs of ligninolysis. Furthermore, higher contents of aromatic C promoted its decomposition under any climatic conditions. We conclude that for a better understanding of aromatic C decomposition and stabilization in soil, it is crucial to consider interactions among climate, litter chemistry, and microbial metabolism. Eco-evolutionary approaches, such as the one proposed here, offer an avenue for capturing these interactions with less complex models that are easier to parameterize.

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### Competing interests

None declared.

### Author contributions

AC and SM conceived the study. AC developed the eco-evolutionary model and performed data fitting with feedback from SM and BDL. AC led the writing. All authors commented, reviewed, discussed the results, and contributed to the writing.

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### Data availability

Data and scripts used to analyze the data are available from doi: [10.5281/zenodo.10553503](https://doi.org/10.5281/zenodo.10553503).

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## Supporting Information

Additional Supporting Information may be found online in the Supporting Information section at the end of the article.

**Fig. S1** Geographical coordinates of litter bag incubation sites in the database.

**Fig. S2** Variation of aromatic C content estimated from NMR spectra of Scots pine litter in relation to the C content of its acid unhydrolyzable residues.

**Fig. S3** Scatter plot of response and predictors in the linear mixed-effect model.

**Fig. S4** Pearson correlation plot between response and predictor variables.

**Fig. S5** Fixed effect estimates for ligninolysis lag time ( $\tau$ ) using a generalized linear mixed effect with zero inflation model using glmmTMB.

**Fig. S6**  $Q_{10}$  estimates of hydrolytic and ligninolytic oxidation rates.

**Fig. S7** Comparisons of simulated ligninolytic oxidation rate with observed ligninolytic enzyme activity.

**Fig. S8** Variation of lag time with initial aromatic C content for varying values of the cost of ligninolytic enzyme production.

**Table S1** Summary of linear mixed-effect model results for the response variables.

**Table S2** Temperature sensitivity index  $Q_{10}$  and activation energy ( $E_A$ ) of hydrolytic and ligninolytic enzymes.

**Table S3** Pairwise  $t$ -test statistics for comparing the significance difference in  $Q_{10}$ .

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